## AIR PERMITTING CASE STUDIES

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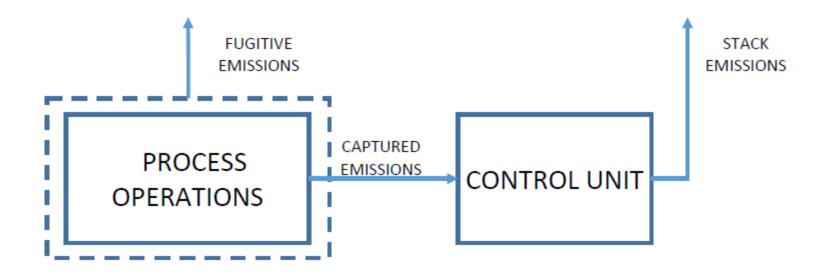


## CASE STUDY #1 "BRUSHING UP" ON BASICS





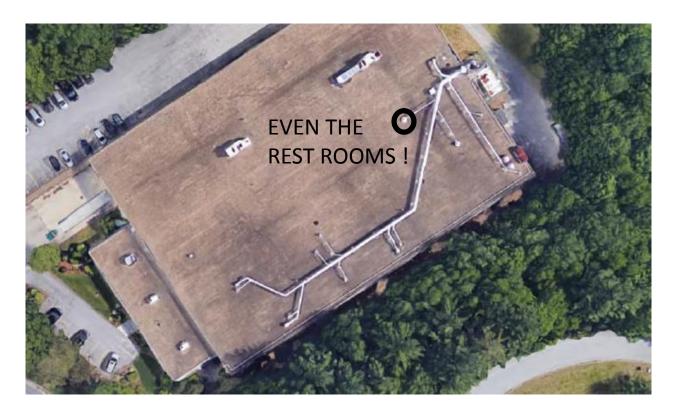
### CAPTURE & CONTROL





### 100 % Capture & 98% Control

METHYL ETHYL KETONE (MEK): VOC +
HAZARDOUS AIR POLLUTANT





### TOXICS USE REDUCTION

 USE OF TOXIC: DILUENT CARRIER FOR ADHESIVE APPLICATION TO POLYURETHANE FOAM

- COMPATABILITY WITH FOAM
- DRYING TIME
- SOLVENCY FOR ADHESIVE
  - ADHESIVE CANNOT BE WATER SOLUBLE



### TUR PLANNING

- PRIMARY ALTERNATIVES
  - SOLVENT INPUT SUBSTITUTION
  - SCRAP REDUCTION BY EQUIPMENT REDESIGN
- COST OF USING
- MEK
  - SOLVENT PURCHASE PRICE
  - SAFETY SYSTEMS FOR FLAMMABLE SOLVENT
  - AIR POLLUTION CONTROL



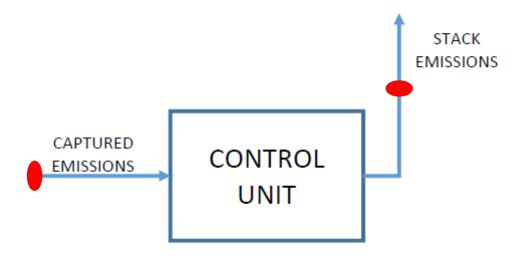
### STACK TEST REQUIRED BY PERMIT

 DESTRUCTION REMOVAL EFFICIENCY (DRE)

<96%

CATALYST REPLACEMENT \$70,000!! FLOW X CONCENTRATION = MASS

$$DRE = \frac{MASS IN - MASS OUT}{MASS IN} \times 100$$





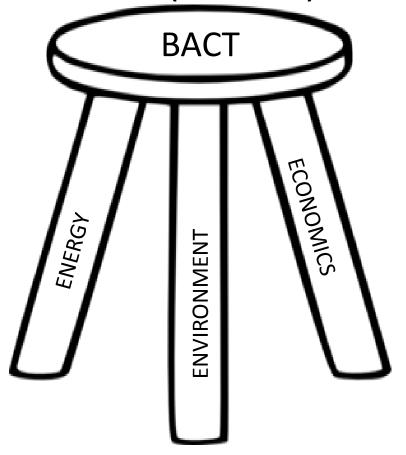
# IF YOU WEREN'T EMITTING VOCs...INPUT SUBSTITUTION BACK ON THE TABLE

### **ACETONE:**

- EXEMPT VOC
  - VOLATILE ORGANIC COMPOUND
  - DOES NOT PARTICIPATE IN SMOG REACTION TO FORM OZONE LIKE OTHER VOCS OR NOx
- TRIALS FIND EFFECTIVE FOR COMPATABILITY WITH FOAM, SOLVENCY AND DRYING TIMES
- FLAMMABLE SOLVENT



## BEST AVAILABLE CONTROL TECHNOLOGY (BACT)





## STOPPING CATALYTIC INCINERATOR

ECONOMICS



\$150,000 PER YEAR SAVINGS ON NATURAL GAS

ENERGY



## STOPPING CATALYTIC INCINERATOR - ENVIRONMENT

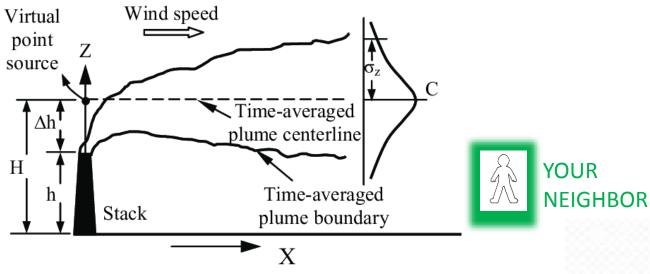
- FUEL COMBUSTION BY-PRODUCTS:
  - CARBON DIOXIDE
  - NOx
  - STILL HAVE TO HEAT BUILDING

REDUCED 95% +



### ENVIRONMENT

NO CONDITION OF AIR POLLUTION



- ACETONE AT PROPERTY LINE
  - NOT ABOVE ALLOWABLE AMBIENT LEVELS
  - NOT ABOVE ODOR THRESHOLD



### BACT APPROVAL OBTAINED

- MassDEP ARBITRARILY RESTRICTED USAGE TO 50
   TONS PER YEAR = 65 PERCENT OF AMOUNT
   PRESENTED AS POTENTIAL TO EMIT IN
   APPLICATION.
- OUT OF THE BOX THINKING PRODUCED COST REDUCTIONS THAT SAVED THE BUSINESS AND JOBS!

# CASE STUDY #2 MANAGEMENT OF CHANGE - SMALL BUSINESS ENDS UP WITH A BIG PERMIT



### BIODIESEL CASE STUDY RECIPE:

- 1. START WITH A HEAPING AMOUNT OF RAPID GROWTH IN A READY MARKET
- 2. ADD A HEALTHY SPLASH OF MISPLACED FAITH IN AN ACADEMIC'S (NOT LICENSED P.E.) ADVICE
- 3. ADD A DASH OF KNOWLEDGE ABOUT ENVIRONMENTAL REGULATIONS
- 4. STIR RAPIDLY WITH VISIT FROM EPA UNTIL MIXTURE BOILS VIOLENTLY

## BIODIESEL PRODUCTION COVERED BY MON NESHAP

- MON MISCELLANEOUS ORGANIC CHEMICAL MANUFACTURING
  - ➤ NESHAP APPLIES IF FACILITY IS A MAJOR SOURCE

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- ➤ MAJOR SOURCE OF HAP IS >=10 TON/YEAR ANY ONE HAP OR >=25 TON/YEAR AGGREGATE HAP
- ➤ METHANOL IS A HAZARDOUS AIR POLLUTANT.

### BIODIESEL PRODUCED BY REACTING USED COOKING OIL WITH METHANOL.

- 1. OIL IS REACTED WITH ACID/METHANOL
- 2. OIL IS REACTED WITH BASE/METHANOL
- 3. BIODIESEL SEPARATED FROM GLYCERIN BY SETTLING
- 4. METHANOL STRIPPED FROM BIODIESEL BY VACUUM
- METHANOL USAGE IS 50+ TON PER YEAR.



### MATERIAL BALANCE ESTIMATES

MEASUREMENT +/- 25% EMISSION OUT ???

BETTER THAN 20:1 RANGE BY DIFFERENCE 3 TO 57 Ton

CONSUMPTION
40 Ton +/- 12 Ton

WASTE OUT
30 Ton +/- 15 Ton

- CHEMICAL ENGINEERING PROFESSOR ASSERTS THAT EMISSIONS ARE "NEGLIGIBLE".
- EPA VISITS AND DOES ENVELOPE CALCULATION OF USAGE AND AMOUNT CONTAINED IN WASTE = DIFFERENCE OF EMISSIONS IS UPWARD OF 30 TONS/YEAR
- FACILITY MONITORS MATERIAL BALANCE MONTH TO MONTH – EMISSIONS RANGE FROM -5 TON TO +60 TON/YEAR.



## EPA AP-42 METHOD FOR CALCULATING EMISSIONS

- VAPOR EQUILIBRIUM FUNCTION OF TEMPERATURE
- ASSUMPTIONS REGARDING COMPOSITION AND IDEAL LAW BEHAVIOR
- WORKING VOLUME AMOUNT DISPLACED W/ FILLING
- (X 0.25 1) EQUILIBRIUM ADJUSTMENT BASED ON FEQUENCY OF TANK TURNOVERS
- BREATHING LOSSES WITH TEMPERATURE CHANGE

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- DOES NOT PREDICT TWO PHASE LIQUID SYSTEMS
- DOES NOT PREDICT VACUUM DISTILLATION PROCESS
- TANK TURNOVER FACTOR FROM API NEVER VALIDATED



### ENGINEERING APPROACH

- STACK TESTING FOR MAGNITUDE ASSESSMENT
  - VENT COMPOSITION X DISPLACED VOLUME
    - WASTE TANK DURING FILLING
    - REACTORS DURING FILL
  - MASS EMISSION MEASUREMENT (CRYOGENIC CONDENSER)
    - VACUUM DISTILLATION (AIR LEAKAGE)
    - REACTORS DURING REACTION
- CALCULATIONS
  - AP-42 SUITABLE FOR RAW MATERIAL TANKS
  - LDAR DEFAULT FACTORS USED FOR EQUIPMENT LEAKS

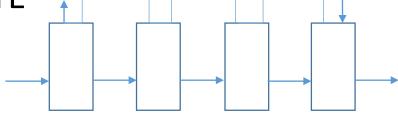


### MAJOR SOURCE DESIGNATION

 WITH GROWTH IN PRODUCTION WHILE ASSESSMENT IS ONGOING ACTUAL EMISSIONS TOP 10 TONS PER YEAR

 REACTOR TANK VAPOR BALANCING COULD HAVE REDUCED ACTUAL EMISSIONS BY 75% FOR COST OF

PIPING – BUT TOO LATE



- MON NESHAP APPLIES
  - 98 PERCENT CONTROL OF HAP PROCESS EMISSIONS

## RECUPERATIVE CATALYTIC INCINERATOR

BURNS PROCESS VENT EMISSIONS 98+% DRE

VFD BLOWER VARIABLE
DILUTION AIR VOLUME
FLOW FOR BED
TEMPERATURE CONTROL

ELECTRIC PREHEATER
NO NATURAL GAS



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### EPA STACK TESTING PLAN ENGINEERING CHALLENGE — INLET FLOW MEASUREMENT



- AFTER DILUTION AIR INTRODUCED THE FLOW IS VARIABLE WITH VFD BLOWER
  - ❖ STANDARD PITOT TUBE CAN'T BE USED (due to variable flow)
  - ❖ FLOW METER PRESSURE DROP TOO HIGH FOR SYSTEM
  - ❖ FLOW PATH TOO SHORT (for turbine meter/needs at least 10 DD)
    MEASUREMENT ERROR +/- 10%

- PRIOR TO DILUTION AIR ENTRANCE
  - ❖ VELOCITY IS TOO LOW TO MEASURE ACCURATELY





### STACK TESTING PLAN

#### PRE-TEST SAMPLING

- CHECK PERFORMANCE OF UNIT BEFORE THE OFFICIAL ENFORCEMENT TESTING FVFNT
  - ❖ PRACTICE FOR PRODUCTION OPERATIONS TO RUN CONCURRENTLY FOR WORST-CASE
  - ❖ EXPERIENCE ACTUAL RANGES OF INLET AND OUTLET CONCENTRATIONS AND TEMPERATURES
  - ❖ SHAKE OUT BUGS IN THE SAMPLING TRAIN WITHOUT EPA WATCHING



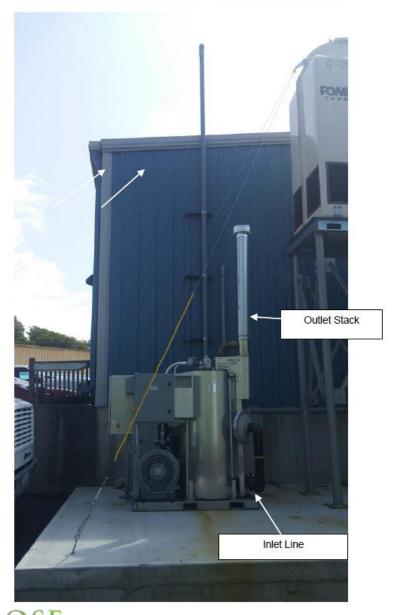


### STACK TESTING PLAN PRETEST COMPOSITION EVAL.

- SIMULTANEOUS INLET/OUTLET SAMPLING
- ESTABLISH METHOD SELECTION WITH EPA
  - IS METHANOL THE ONLY VOC/HAP?
  - NCASI 98.01 combined with TO-15
- OBTAIN CALIBRATION GAS (CH4) AT SUITABLE CONCENTRATION (10,000ppm inlet / 100ppm outlet)
- Methanol cylinder purchased to determine response factor (0.802 RF) allowing for comparison to alternative limit to DRE of <20ppmvd@3%O2 as methanol.

Result: Methanol represented 97.66% by mass of all compounds VOCs. Method 25A suitable for DRE.

Figure 3-2 Picture of Test Locations - Oxidizer Inlet and outlet



#### STACK TESTING PLAN

#### **PROCESS CHARACTERIZATION**

- HOW TO ESTABLISH WORST-CASE CONDITIONS FOR TESTING ON BATCH DRIVEN OPERATION (10 scenarios identified which were expected to yield majority of emission episodes)
- SCHEDULE PRODUCTION OPERATIONS TO RUN CONCURRENTLY FOR WORST-CASE
- NON-ROUTINE OPERATION SAFETY REVIEW





## EPA STACK TESTING PLAN Elimination of Flow Measurements (Concentration based DRE)

Irwin Engineers was able to demonstrate through calculation to EPA that inlet and outlet flow would be within 1% while actual flow measurements would likely yield an error of 10% or more due to variable flow rates, low flow rates and poor sampling locations.

As such, VOC DRE was allowed to be calculated based on a ppmvd corrected to a 3% basis. This required simultaneous measurement of VOC, O2 and moisture.

Compliance test yielded a 99.5% VOC/HAP DRE.





### **EPILOGUE**

- AFTER IMPLEMENTING PROCESS
   CHANGES FOR VENTING AND OXIDIZER
   CONTROL THE ACTUAL EMISSIONS OF
   METHANOL WERE LESS THAN 3 TONS
   PER YEAR.
- LARGEST COMPONENT OF ACTUAL EMISSIONS = EQUIPMENT LEAKS
- METHANOL NOW BEING 100%
   RECYCLED BY DISTILLATION ON-SITE
- PRODUCTION CAN INCREASE 10X
   WITHOUT EXCEEDING 10 TONS
- AFTER EPA REVERSAL OF ONCE-IN-ALWAYS-IN POLICY RIDEM IS REPERMITTING THE FACILITY AS A MINOR SOURCE.

